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¹ Validation of a method for extracting microplastics

² from complex, organic-rich, environmental

3 matrices

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8

9 ABSTRACT

10 Complex and organic-rich solid substrates such as sludge and soil have been shown to be contaminated by microplastics; however, methods for extracting plastic particles have not yet been systemically tested 11 or standardised. This study investigated four main protocols for the removal of organic material during 12 analysis of microplastics from complex solid matrices: oxidation using H₂O₂, Fenton's reagent, and 13 alkaline digestion with NaOH and KOH. Eight common polymer types were used to assess the influence 14 15 of reagent exposure on particle integrity. Organic matter removal efficiencies were established for test 16 sludge and soil samples. Fenton's reagent was identified as the optimum protocol. All other methods 17 showed signs of particle degradation or resulted in an insufficient reduction in organic matter content. A further validation procedure revealed high microplastic extraction efficiencies for particles with 18 19 different morphologies. This confirmed the suitability of Fenton's reagent for use in conjunction with 20 density separation for extracting microplastics. This approach affords greater comparability with existing studies that utilise a density-based technique. Recommendations for further method 21 optimisation were also identified to improve the recovery of microplastic from complex, organic-rich 22 environmental samples. 23



26



28 Introduction

29 Microplastic contamination has emerged as a major global environmental issue. Small plastic particles are now pervasive across marine and freshwater systems^{1–5}. Recently, attention is beginning to focus 30 on the occurrence of microplastics within other environmental compartments⁶. Wastewater treatment 31 plants (WWTPs) have been shown to have a high trapping efficiency for microplastics^{7,8}. However, 32 particles are concentrated in the solid sludge phase^{8,9}, which is often applied to agricultural soils as 33 fertiliser. Nizzetto et al.¹⁰ estimate that between 63,000-430,000 and 44,000-300,000 tons of 34 microplastic are added per year to farmlands in Europe and North America respectively. Hence, 35 agricultural soils may represent a major environmental reservoir of microplastic. A small number of 36 studies have examined microplastics in soil^{11–14} and sludge samples^{7–9,15–21}, but no standardised method 37 38 has emerged. The organic components, complexity of the solid matrix, and presence of additional contaminants complicates the extraction of small plastic particles²². Accurately assessing the magnitude 39 of temporary stores, source inventories and emission rates of microplastics in terrestrial environments 40 41 is crucial for the definition of management frameworks and the protection of both terrestrial and marine systems. There is an objective urgent need for validated analytical methods to effectively characterise 42 43 microplastic dynamics in this specific area.

The majority of work extracting microplastics from solid matrices has been concerned with aquatic 44 sediments. Most commonly, microplastics are extracted based upon their density²³⁻²⁵. This can be 45 performed using density solutions or through elutriation-based methods^{26,27}. However, this approach, 46 when used alone, is not effective for the analysis of microplastics in sewage or soil samples based on 47 48 the high organic matter content (up to 99%) and the presence of complex organic compounds and aggregates. For example, soil organic matter (SOM) typically exhibits a density of 1.0 - 1.4 g cm⁻³ and 49 therefore will not be effectively separated from microplastics during density extraction²². Hence, 50 51 additional procedural steps are required.

Preliminary studies that have examined small quantities of *sewage sludge* have bleached, dried, or filtered samples prior to analysis^{8,9,16,17}. This approach is not sufficient for analysing larger sample sizes, where the organic component will likely physically conceal microplastic particles during identification and quantification. More recently, studies have applied density-based separation^{9,17–20}. Some studies have incorporated an organic matter removal step^{19,20}; however, the efficacy of these techniques has not yet been systematically tested.

In contrast, analyses of microplastic in soil samples have, thus far, concentrated on direct extraction 58 techniques, such as pressurised liquid extraction¹³, thermal decomposition coupled with GC-MS^{11,14}, 59 and rapid heat treatment²⁸. These approaches negate the need for sample pre-treatment (i.e. the isolation 60 61 of microplastic particles) and yield mass-based concentrations of common polymer types. However, they destroy particle information that is critical to current microplastic research directives e.g. particle 62 numbers, shapes, and size. These details are presently more important for establishing potential sources 63 64 or associated ecotoxicological implications than polymer concentration alone. As discussed by Fuller and Gautam¹³, these approaches will likely complement existing methods. 65

66 The lack of a standardised approach to microplastic analysis has already been widely discussed^{24,29}. An
67 important additional note is the current lack of a sufficiently detailed, unique classification scheme for
68 microplastics and related reference materials needed for the validation of methods. This is for example
69 the case for microfibers, car tire debris and other types of microplastic.

This study aims to identify an additional processing step that can be added to existing methods for analysing microplastic in solid substrates (e.g. aquatic sediments). Namely, the removal of organic material from soil and sludge samples will be tested. Eerkes-Medrano et al.³⁰ highlighted several considerations for methodological development: techniques should be simple, affordable, precise, accurate, and have limited potential for contamination. This study will test four main protocols to establish the optimal method for extracting microplastics from organic-rich environmental substrates which satisfies these criteria.

77

78 Methods

79 <u>Review of existing organic matter removal techniques</u>

80 A commonly applied technique for removing organic material from environmental matrices is oxidation 81 using hydrogen peroxide (H_2O_2). Despite this, the efficacy of H_2O_2 has been called into question. Cole et al.³¹ found that only 25% of *biogenic* material was removed following treatment with 35% H₂O₂ at 82 ambient temperature for 7 days. This has been observed elsewhere, where hydrogen peroxide often has 83 the effect of bleaching organic material rather than completely removing it ³². Additionally, Nuelle et 84 al.³² noted the degradation of some polymer types as a result of H₂O₂ oxidation. These included 85 polyethylene (PE) and polypropylene (PP), which are amongst the most commonly produced plastics 86 87 globally. Despite this, further studies have observed no significant changes to microplastic particles following H_2O_2 digestion, including no evidence of microplastic bleaching^{20,33}. To reduce the reaction 88 89 time, some studies have utilised higher temperatures during peroxide oxidation. For example, Sujathan et al.²⁰ used 30% H₂O₂ at 70°C to decrease the reaction time to approximately 12 hours. Whilst 70°C is 90 91 lower than the continuous operating temperatures (COTs) for most of the common polymer types, the authors noted that particles composed of PMMA may be affected²⁰. A modified approach using lower 92 temperatures may overcome this issue, although the effect on reaction time must be assessed. 93

94 A potential alternative to peroxide oxidation is the use of Fenton's reagent. This has previously been
95 used to extract microplastics from organic-rich wastewater samples³⁴. Fenton's reagent is an advanced

oxidation process using H_2O_2 in the presence of a catalyst (Fe²⁺). This method is performed at ambient 96 temperature, reducing the potential for exceeding COTs. Fenton's reagent is effective in destroying 97 organic components such as highly chlorinated aromatic compounds or inorganic compounds, which 98 are typically recalcitrant in $H_2O_2^{35,36}$. This may prove more effective in removing all organic 99 components from complex environmental substrates. Additionally, the reaction occurs more rapidly 100 than traditional H₂O₂ oxidation, typically taking less than 1 hour to process wastewater samples³⁷. 101 Ferrous sulfate (FeSO₄·7H₂O) is usually used as the iron catalyst component and is inexpensive and 102 readily available. Although, the composition of sewage sludge may reduce the efficacy of organic 103 matter removal; high concentrations of hydroxyl free radical scavengers, for example, will inhibit the 104 degradation of organic material³⁸. Furthermore, the pH of the reagent must be adjusted (to 3.0 - 5.0) to 105 encourage the dissolution of the ferrous sulfate granules and optimise the degradation of organic 106 material³⁹⁻⁴¹. This acidity may begin to degrade some polymers, although this effect was not observed 107 by Tagg et al.³⁴. Therefore, the efficacy of this technique needs to be tested. 108

109 Other potential methods for the removal of organic matter arise from existing studies that extract microplastics from biota. Acid digests, such as hydrochloric acid (HCl) and nitric acid (HNO₃), have 110 been shown to be highly effective in destroying organic matter but they also attack microplastic 111 particles, leading to degradation and melting^{31,33,42}. Hence, these have not been considered further. 112 Alkaline digests have also been investigated, including potassium hydroxide (KOH) and sodium 113 hydroxide (NaOH). Dehaut et al.42 showed that use of 10 M NaOH led to the degradation of 114 polycarbonate and polyethylene terephthalate; however, Mintenig et al.¹⁹ used NaOH digestion to 115 remove organic material from sewage sludge samples. 10% KOH at 60°C has been highlighted as the 116 optimum procedure for the extraction of microplastics from *biota* ^{33,42–45}. However, the efficacy of KOH 117 in extracting microplastics from *sludge* or *soil* must be tested. KOH breaks down humic acids; however, 118 Bläsing and Amelung²² point out that humins and alkali-insoluble compounds within soils will not be 119 120 removed. Humins are likely to also be present in sewage sludge in the form of raw organic matter, bacteria, and fungi that may not been removed by the wastewater treatment process⁴⁶. Therefore, testing 121

of this procedure on complex environmental samples is important to establish the degree of organicmatter removal in this context.

Finally, a number of studies utilise enzymatic digestion to remove organic material prior to microplastic 124 analysis. Cole et al.³¹ first introduced the use of proteinase-K to extract microplastics from both seawater 125 and biota. They report a removal of >97% of biogenic material present. However, this technique was 126 applied on small sample volumes (0.2 g dry weight) and the enzyme used is expensive. Hence, it may 127 not be feasible or cost-effective to process large samples with high organic content using this technique. 128 Likely, a range of enzymes will be required to breakdown the different organic compounds found in 129 these sample types. Mintenig et al.¹⁹ apply an enzymatic-oxidative procedure to extract microplastics 130 from wastewater samples. They used protease, lipase and cellulase, which are less expensive than 131 proteinase-K. However, the procedure took over six days to complete and the same study goes on to 132 utilise a different, non-enzymatic, approach to analyse sludge samples. This suggests that the technique 133 134 may not be optimised for analysing solid environmental samples. For these reasons, enzymatic treatments were not tested in this study. 135

136

137 <u>Experimental design</u>

The majority of studies that analyse microplastics in solid samples (e.g. sediments) utilise a density separation procedure to isolate microplastic particles^{23,24}. To increase potential for comparability, the aim of this study was to add an additional processing step to remove organic matter in conjunction with a density separation approach. Based on the review of existing literature, four main protocols were tested for removal of organic material from complex, organic-rich, environmental samples. Temperature and concentration variants were also tested for some of the selected reagents. As a result, this study tested a total of six protocols:

145 1. **30% (v/v)** H_2O_2 . Sujathan et al.²⁰ used this reagent at 70°C; however, the authors noted that 146 this may be above the COTs of some polymers. Microplastics have been shown to be preserved

- 147 by other reagents during continuous heating at $60^{\circ}C^{42}$. Hence, this protocol was tested at two 148 temperatures:
- a. 30% hydrogen peroxide at 70°C
- b. 30% hydrogen peroxide at 60°C
- Fenton's reagent. This reagent has two components: 30% (v/v) H₂O₂ with an iron catalyst.
 The catalyst solution was composed of 20 g of iron (II) sulphate heptahydrate in 1 l of filtered
 RO water. Tagg et al.³⁴ tested this reagent within the context of extracting microplastics from
 wastewater. The authors identified this as the optimum concentration. The catalyst solution was
 adjusted to pH 3.0 using concentrated sulfuric acid.
- NaOH solution. A 10 M solution has been applied to sludge samples by Mintenig et al.¹⁹, although studies have identified some particle degradation with this concentration⁴². A lower concentration solution may present a reduced potential for particle degradation. This technique has previously been used at different concentrations to extract microplastics from biota^{31,47,48}. Hence, this protocol was tested at two concentrations to observe differences in microplastic preservation and organic matter removal:

162 a. 1 M NaOH at 60°C

163 b. 10 M NaOH at 60°C

164 4. 10% KOH solution at 60°C. This protocol has been rigorously tested within the context of
 biota microplastic studies⁴². The optimal operating conditions (10%, 60°C) were applied here
 166 to test the efficacy of this technique in removing organic material from soils and sludge.

Protocol assessment was split into two main phases: 1) testing the effect of the selected protocols on plastic particles; and 2) establishing the efficacy of the protocols in removing or reducing organic matter content. Method validation was performed by assessing the extraction efficiency of the optimum protocol. The optimum protocol was established by the outcomes of Phase 1 and 2 testing. A schematic diagram showing the experimental design is provided in Figure S1.

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173

174 Phase 1: Effect of reagents on polymeric particles

The initial testing phase aimed to establish the preservation of microplastics following exposure to the reagents. Eight common polymer types were tested for indicators of degradation following treatment: PP, LDPE, HDPE, PS, PET, PA-66, PC, and PMMA (Table S1). These represent >70% of plastic demand in Europe⁴⁹. Details of the particles used are provided in Table S2 and images are presented in Figure S2. The test particles were acquired through the JPI-Oceans BASEMAN project. The tested particles represent large microplastics. Particles of this size were tested to improve the quality of weight and mass measurements and to afford greater visibility of degradative changes to the particle surface.

182 Three replicates were analysed for each of the six protocols, in addition to three control samples. Three 183 particles from each polymer type were tested in each replicate (total of 504 particles tested). The 184 particles were placed into clean, pre-washed glass jars and 30 ml of each reagent was added. Filtered RO water was used in the case of the control samples. Protocols 1a, 1b, 3, 4 were placed into an 185 incubator (60 or 70°C, as detailed above; 120 rpm). The samples for Protocol 2 and the control samples 186 187 were performed at room temperature. The particles were exposed to the reagents for 24 hours. They were then removed from the jars, rinsed thoroughly in filtered RO water, and left to air dry in petri 188 dishes. 189

Microplastic particles were characterised physically prior to and following exposure. Each particle was measured along the a- and b-axis using a Nikon SMZ 745T stereomicroscope at 10x magnification and the Infinity Analyse software package. Particle mass was also recorded before and after treatment. Each particle was photographed to assess for any visual evidence of degradation. Some particles exhibited surface degradation following treatment (see Results and discussion). In this case, the particles were first photographed and then gently brushed to remove loose fragments prior to taking mass and size measurements.

Following treatment, three particles of each polymer type from each treatment were analysed using FT-IR (n = 168). Particles were tested using an Agilent Cary 630 FT-IR spectrometer with a diamond ATR accessory. Spectral changes were noted, in addition to deviations in the library search hit quality index. The library search was performed using the Agilent Polymers ATR library. Matches were calculated by the MicroLab PC software which uses a scalar product algorithm to assign a hit quality index. For particles exhibiting surface degradation, the fragments from the outer layer were analysed separately to test for differences in the FT-IR spectra.

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205 Phase 2: Efficacy of reagents in reducing organic matter content

The second phase of testing aimed to establish the proportion of organic material that is removed by each of the selected protocols. For this experiment, test soil and sludge samples were collected from the Oslo area. Details of sample characteristics including sampling, soil texture analysis and sludge treatment are provided in the Supporting Information. Moisture content was established through the percentage loss following drying at 105°C. The organic matter content of the samples was assessed through loss-on-ignition (LOI): the samples were placed into a muffle furnace and heated to 550°C for 4 hours. The results are provided in Table S3.

10 g of soil and sludge were weighed into clean, pre-washed glass jars. Three replicates were performed 213 for both sample types, for each protocol (n = 36). The samples were first dried at 105°C to establish the 214 dry weight. For Protocols 1 and 2, 30 ml of H₂O₂ was added initially, followed by further additions in 215 5 ml increments until no further reaction (e.g. fixing, frothing) was observed. In the case of Protocol 2, 216 the reagent was added as a ratio 1:1 H₂O₂ and catalyst solution. The catalyst solution was added first 217 218 and H₂O₂ was then added slowly. Further additions of the reagents were added until no reaction was observed. The samples were processed at room temperature, but an ice bath was used to modulate the 219 220 temperature when it exceeded 40°C (Protocol 2 only). For Protocols 3 and 4, 50 ml of reagent was 221 added, with no further additions during the reaction period.

Following organic matter removal, the overlying liquid was decanted and vacuum-filtered onto preweighed Whatman GF-D filter papers. The filter paper was dried and the retentate mass was established gravimetrically. The total mass loss (Δ m) was assumed to directly reflect the loss of organic material and this was used to estimate organic matter removal (%). 226

227 <u>Validation: Extraction efficiency of selected protocol</u>

The final phase of testing included establishing the extraction efficiency of the optimum protocol, which
was identified following Phase 1 and 2 testing. This aimed to assess whether the additional processing
step affected the recovery of particles during the full microplastic extraction procedure.

The test sludge and soil used in this study represent environmental samples. Three control samples of sludge and soil were first tested for existing microplastic concentrations using the selected protocol. Microplastic abundance in both samples was low and no particles with similar physical characteristics (size, colour) were observed. The results and description of measurements are provided in the Supporting Information.

236 Different microplastic shapes were used to test the influence of particle shape on extraction efficiency. Thirty large PE microbeads (850-1000 µm), 30 small PE microbeads (425-500 µm), and 30 PET fibres 237 (322-395 µm) were added to each replicate. Details on the particles are provided in Table S4 and images 238 are shown in Figure S3. Orange fibres (Certified reference material CRM-FOPET-1-18, NIVA, 239 240 Norway) were used to spike the solid samples. No orange clothing or textiles were permitted near the samples during testing to prevent artificially enriching samples through airborne contamination. No 241 orange fibres were observed in ongoing laboratory contamination tests. All sample processing was 242 performed in a sterile cabinet and samples were kept covered to prevent laboratory contamination. Only 243 244 fibres within the predefined size range were considered, although no smaller or larger orange fibres were identified. 245

For each replicate, 10 g (d.w.) of sample (sludge/soil) was added to clean, pre-washed glass jars. The samples were then spiked with the microplastic particles. The particles were thoroughly mixed into the solid matrix. Samples were then partially wetted using a fine spray of filtered RO water and allowed to air dry. This was repeated three times to encourage the incorporation of microplastic particles into aggregates. This aimed to mimic environmental samples and establish environmentally-relevant extraction efficiencies. 252 Organic matter removal followed the same method as outlined in Phase 1 & 2. Only the optimal protocol underwent validation. Density separation was achieved using a) filtered RO water, to extract 253 microplastics at freshwater density (1 gm cm⁻³); and b) NaI solution (1.8 g cm⁻³), to extract higher 254 density microplastics. Sequential density extractions have been applied elsewhere to infer the potential 255 256 environmental behaviour of particles⁵. Containers were filled to the top with each density solution, sealed, and agitated for 1 minute. The supernatant was decanted after the sample had been allowed to 257 258 settle for 24 hours, and vacuum filtered through Whatman GF-D filter papers. Once air-dried, the filter 259 papers were traversed at 20x magnification to count the extracted microplastics.

Several analytical parameters associated with density separation were tested. Firstly, the importance of the ordering of the analytical procedure was investigated. Extraction efficiencies were established for a) organic matter removal followed by density separation (OMR \rightarrow Density); and b) density separation followed by organic matter removal (Density \rightarrow OMR). Three replicates were tested for both approaches. For the 'Density \rightarrow OMR' samples, the filter papers were placed into a jar after density separation and subjected to organic matter removal. The samples were then filtered again, and the original filter paper was carefully rinsed to ensure all particles were passed through the second filter.

Secondly, the optimum number of density extracts was examined. Three density extracts were performed for each density solution and the number of particles isolated in each was recorded. Finally, the labware used for density separation was tested. Three replicates were tested in 250 ml glass jars that were used in the previous phases and three additional replicates were tested using 50 ml tubes. For the latter, the 'OMR \rightarrow Density' samples were transferred to the tubes prior to density separation (organic matter removal was always performed in glass labware).

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277 Results and discussion

278 Phase 1: Effect of reagents on polymeric particles

279 Physical changes

Different protocols to remove organic material had different effects on the physical integrity of the 280 polymers. In one replicate of Protocol 1b (30% H₂O₂ 70°C), all three PA-66 particles were destroyed. 281 282 Small residual fragments were observed during filtering (Figure S4). This outlier had considerable 283 influence on the average and variance of mass and size changes observed for this treatment (Table 1). The particles in the other two replicates for that treatment showed no signs of degradation. The reason 284 for such a different outcome is unexplained. PA-66 is not resistant to hydrogen peroxide at 285 concentrations $\geq 30\%^{50}$, which causes oxidative damage and degradation of the polymer structure. 286 However, the exposure time of the three peroxide-based treatments (Protocols 1a, 1b, and 2) appears to 287 be below the time required to have an observed effect on particle mass, size, or visual appearance. 288 However, the temperature setting (70°C) used in Protocol 1b may just exceed the threshold tolerance 289 290 of PA-66 particles.

In all three replicates performed for Protocol 3b (10 M NaOH), PET and PC particles were severely 291 degraded. Surface degradation was observed for both polymer types (Figure 1bc). These visual changes 292 293 were also recorded as significant decreases in particle mass and size (Table 1). This effect was observed 294 to a lesser extent for Protocol 3a (1 M NaOH), with signs of 'peeling' (PET) and the development of a 295 matte texture (PC) (Figure S5). However, no significant change in mass or size was measured. Notably, 296 a decrease in weight of 16.1% was observed for PC following treatment with 10% KOH (Protocol 4), 297 despite no associated visual or size-related changes. Polycarbonate is significantly affected by hydrolytic degradation, and alkali salt solutions such as NaOH (Protocol 3a,b) and KOH (Protocol 4) 298 accelerate this process⁵¹. Alkaline solutions also degrade PET by saponification of ester linkages at the 299 particle surface⁵², although this was only observed for NaOH-based treatments in this study. 300

For PP treated with Protocol 1b ($H_2O_2 70^{\circ}C$), one particle in a single replicate was significantly reduced in size and coated with an opaque white layer (Figure 1a). This degradation may have been catalysed by the destruction of PA-66, which occurred in the same single replicate. All other PP particles wereunaffected by the Protocol 1b treatment.

Some limited surface degradation, noted as 'crazing', was observed for PS particles following treatment with hydrogen peroxide (Protocols 1a and 1b) (Figure 1de). Protocol 2 (Fenton's reagent) also uses hydrogen peroxide but no degradation was observed (Figure 1f). This may be linked to the influence of temperature, where more degradation was observed following Protocol 1b (70°C) than Protocol 1a (60°C). Oxidation of polystyrene occurs in air when temperatures are elevated⁵³. Protocol 2 was performed at temperatures <40°C.

Interestingly, an increase in the weight of PS following treatment with 10% KOH (Protocol 4) was measured. This does not correspond to any size or visual changes. This effect was not observed during other methods testing studies⁴², but could influence the density of the particle and effect subsequent microplastic extractions based upon density. The authors were not able to identify the cause of this change during testing.

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317 <u>Spectral changes</u>

The majority of the post-treatment FT-IR results exhibited no major deviations from the control samples 318 (Figure S6). The only significant alteration is observed for PC following treatment with Protocol 3b. 319 320 The alkaline hydrolysis appears to have initiated depolymerisation, demonstrated by the introduction of 321 breakdown products to the spectrum. The same spectrum is produced when analysing the degraded outer layer as well as the newly-exposed surface of the particle (Figure S6g and S7c). The degradation 322 of PET caused by the Protocol 3b did not alter the FT-IR spectra of the particle. However, the loose 323 324 fragments taken from the surface of the degraded particles had altered FT-IR spectra (Figure S7). Some 325 reduction in intensity is observed for PA-66 following a range of treatments; however, this is likely associated with variations in the polymer structure of the virgin particles. 326

Library searches were performed for each analysed particle. With the exception of PC followingProtocol 3b, all particles were successfully matched to the correct reference spectra with satisfactory

hit quality index (HQI) scores ≥ 0.88 (on a 0-1 scale). The loose fragments taken from the degraded particles all recorded deviations from the control spectra. The spectra from the degraded PC and PET fragments could not be reliably matched to any compound in the library, with HQIs <0.30. However, fragments from the single PP particle that was affected by Protocol 1b, which developed a white outer layer, matched with polyamide (HQI = 0.90). In the same replicate, PA-66 was destroyed. The solubilised fragments apparently adhered to the outside of the degraded PP particle, which would have led to the incorrect characterisation of the particle if the degraded layer had not been removed.

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337 Phase 2: Efficacy of reagents in reducing organic matter content

338 Table 2 shows the total average mass loss (Δm) and organic matter removal of soil and sludge samples following treatment with the selected protocols. For both sludge and soil, peroxide-based treatments 339 removed significantly more of the organic material than the alkali salt solutions (Table 2). Peroxide 340 oxidation is already used to reduce the organic content of solid environmental samples prior to other 341 342 analyses. For example, 30% hydrogen peroxide is commonly used to pre-treat samples before measuring particle size distribution^{54,55}. However, the completeness of peroxide digestion of organic 343 material varies based on the composition of the organic content⁵⁶. In this study, peroxide-based 344 345 treatments (Protocols 1a, 1b, & 2) removed approximately 80-87% of the organic content of the sludge 346 samples and 96-108% of soil organic material (Table 2). The higher temperature used in Protocol 1b appears to have improved the removal efficiency of the treatment. Fenton's reagent achieved 347 comparable removal rates to the 70°C hydrogen peroxide treatment. This removal may have been 348 enhanced by the low pH of the reagent, which introduces optimal conditions for the treatment of 349 organic-rich samples such as soil⁵⁷. 350

Treatment with alkaline salt solutions (Protocols 3a, 3b, & 4) removed between 57-67% of organic material in sludge and 35-68% of soil organic matter. Alkaline hydrolysis is effective at destroying proteins³¹, which is why it is commonly utilised for the extraction of microplastics from biota. In contrast, cellulosic and chitinous material is resistant to KOH and NaOH treatment⁵⁸, and may be present in both sludge and soil. Additionally, alkali-insoluble humins are often the most abundant organic fraction found in soils⁵⁹. This explains the lower removal efficiencies of NaOH and KOH. The higher percentage of organic matter removal by 10% KOH in sludge than in soil may reflect the composition of organic material within the test samples.

359

360 <u>Critical selection of optimal clean-up method</u>

Based on the results of Phase 1 testing, Protocols 1a, 2, and 4 could be considered to preserve 361 microplastics satisfactorily, causing minimal to no damage. Only the use of Fenton's reagent (Protocol 362 2) did not cause any observed changes to the eight tested polymer types. Phase 2 testing showed that 363 the use of alkaline salt solutions is not appropriate for the removal of organic material in complex, 364 organic-rich, environmental matrices. In contrast, Protocols 1b and 2 were the most effective at reducing 365 organic material. However, Protocol 1b caused degradation of several polymer types during Phase 1 366 testing. Based on these outcomes, Fenton's reagent was identified as the optimum protocol for 367 368 preserving microplastic particles whilst also effectively reducing the organic components of soils and sludges. 369

370 This study highlights the unsuitability of NaOH as a reagent for removing organic matter in microplastics studies. Based on the degradation of multiple polymer types, it is recommended that 371 NaOH is no longer used for microplastic analysis. Dehaut et al.⁴² reported similar effects on PET and 372 PC following treatment with 10 M NaOH, however, this study demonstrates that lower concentrations 373 of this reagent (1 M NaOH; Protocol 3a) still exhibit surface degradation in these polymer types. Thus 374 far, NaOH has only been used in a single study of microplastic contamination in sludge samples by 375 Mintenig et al.¹⁹. However, in this case, the authors highlight that the method was as yet untested and 376 377 microplastic results were subsequently presented as estimates.

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381 <u>Validation: Extraction efficiency of selected protocol</u>

The validation phase focused on assessing the recovery of microplastics following treatment with the 382 selected optimal protocol: Fenton's reagent. Figure 2 shows extraction efficiencies for the spiked 383 384 microplastic particles. The ordering of the analytical procedure (organic matter removal followed by 385 density separation, and vice versa) had no significant effect on the recovery of the different microplastic particles. Hence, the organic matter removal step can be added within existing protocols for microplastic 386 isolation through density separation based on preference or convenience. The overall extraction 387 efficiencies were very high. Large PE beads had close to 100% recovery for both the sludge and soil 388 389 test. Small PE beads were also mostly recovered, with extraction efficiencies between 92-98%. The 390 spiked PET fibres presented the lowest recovery (79-86%) but this was still considered to be satisfactory. These results are higher than or comparable to the extraction efficiencies observed 391 following density separation alone by Claessens et al.²⁶. Hence, the inclusion of an organic matter 392 removal step using Fenton's reagent does not negatively affect the recovery of microplastic particles 393 394 from complex, organic-rich, environmental matrices. Only low density microplastics (small and large PE beads) were observed in the freshwater density extracts, whilst only PET fibres were extracted 395 during the subsequent NaI steps. Crucially, no evidence of degradation was observed for the spiked 396 397 microplastic particles following treatment, confirming observations during phase 1 testing.

There is no difference between the recovery of small or large PE beads using either 250 ml glass jars 398 399 or 50 ml tubes (Table S5). However, the extraction of fibres is slightly increased by using the tubes. Extraction efficiencies when using jars were 76-78%, compared to 79-86% for the tubes. The lower 400 401 recovery of irregularly-shaped particles, such as fibres, during density separation is often speculated as the effect of particles adhering to the walls of the apparatus^{32,60}. These results indicate that this is likely 402 403 to be a contributing factor, whereby the container with the smallest internal surface area led to higher 404 recovery of fibres. Furthermore, there was no significant difference between the ordering of the 405 analytical procedure for either container. Hence, methods which have been shown to have high 406 extraction efficiencies for a range of particles types^{26,27,61}, may also be used for soil and sludge samples
407 in conjunction with an organic matter removal step.

During the density separation procedure, three extracts were processed for both density solutions (low, 408 freshwater density: 1 g cm⁻³ & high density 1.8 g cm⁻³). The recovery data for the different particle types 409 associated with each extract are provided in Table S6. For low density microplastics (PE beads), the 410 majority were recovered in the first extraction. The extraction efficiencies for large PE beads was close 411 to 100%, whilst the mean recovery of small PE beads after one extraction was 87.2%. For higher density 412 PET fibres, only 50.8% of particles, on average, where extracted in the first step. A further 28.6% were 413 414 recovered in the second extract. This may relate to the adhesion of particles to the inside of the tubes during decanting, which are then successfully recovered in a second extract. Alternatively, the settling 415 of the solid matrix may trap higher density particles with complex shapes and prevent them from 416 floating to the surface of the density solution. Very few particles of any type were recovered in the third 417 418 extract (<4.4%). Based upon this testing, it is recommended that two extracts are taken for each density solution used to ensure optimal recovery of microplastic particularly for higher density 419 extractions (e.g. NaI or ZnCl₂). Performing a third extract may slightly increase recovery of plastics 420 from environmental samples; however, the use of two extractions for each density solution represents 421 422 a more time-effective approach that is capable of recovering the majority of plastic particles.

423

424 Method optimisation

Organic matter removal using Fenton's reagent is an exothermic reaction. Reaction temperatures in the context of organic matrices can reach as high as 89°C⁶². This may negate the benefit of using Fenton's reagent, where degradation of polymers was observed for peroxide-based treatment performed at 70°C in Phase 1 testing (Protocol 1b). However, an ice bath can be used to lower the reaction temperature. This can also limit the occurrence of violent reactions improving safety conditions in the laboratory. It is recommended to keep the temperature below 40°C to decrease the decomposition of hydrogen peroxide⁴⁰. This will also better preserve microplastic particles. During testing, reactions using Fenton's reagent were completed in less than 2 hours for both sludge and soil samples when using an ice bath
 intermittently to adjust reaction temperatures⁶³.

As stated previously, the optimal pH for Fenton's reagent is close to 3.0. However, it is important to
monitor the pH of the reaction, as if it exceeds pH 5-6, an iron hydroxide precipitate will form. This
precipitate floats out during density separation and hinders visual analysis and chemical characterisation
through physical obscuration. Although, during the testing of sludge and soil samples, this effect was
not observed.

Fenton's reagent represents an effective, low-cost, and rapid treatment for removing organic material from complex, organic-rich environmental matrices. Coupled with density separation, the majority of microplastics are recovered, where the organic matter removal step does not significantly affect extraction efficiencies compared to other solid matrices.

443

444 FIGURES:



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Figure 1. Micrograph (10x) images of selected plastic particles before (top) and after (bottom)
treatment. Small pitting in the surface of PS granule was observed for Protocols 1a (d) and 1b (e), but
not following treatment with Protocol 2, which also utilises hydrogen peroxide as an oxidising agent
(shown in the magnified images).

Table 1. Changes in mass (a) and size (b) of the tested plastic particles following treatment. Results are presented as the mean \pm SD of the three replicates per treatment (3 particles per replicate). Significant changes, defined as a change greater than analytical error (\pm 10%), are highlighted in bold.

a. Mass

	Protocol 1a H ₂ O ₂ (60°C)	Protocol 1b H ₂ O ₂ (70°C)	Protocol 2 Fenton's reagent	Protocol 3a 1 M NaOH	Protocol 3b 10 M NaOH	Protocol 4 10% KOH	Control
РР	$-0.11\% \pm 0.16\%$	-5.96% ± 8.52%	$0.14\% \pm 0.11\%$	$-0.16\% \pm 0.14\%$	$0.18\% \pm 0.26\%$	$-1.30\% \pm 1.31\%$	$0.27\% \pm 0.10\%$
LDPE	$-0.05\% \pm 0.28\%$	$0.00\% \pm 0.00\%$	$-0.05\% \pm 0.20\%$	$0.00\% \pm 0.14\%$	$0.01\% \pm 0.14\%$	$-2.39\% \pm 2.78\%$	$0.17\% \pm 0.01\%$
HDPE	$0.07\% \pm 0.05\%$	$-0.01\% \pm 0.17\%$	$0.07\% \pm 0.05\%$	$0.03\% \pm 0.05\%$	$\textbf{-0.10\%} \pm 0.01\%$	$0.07\% \pm 0.05\%$	$0.07\% \pm 0.05\%$
PS	$0.06\% \pm 0.09\%$	$-0.01\% \pm 0.24\%$	$0.00\% \pm 0.14\%$	$-1.81\% \pm 2.44\%$	$0.16\% \pm 0.13\%$	$12.1\% \pm 2.08\%$	$-0.89\% \pm 1.13\%$
PET	$0.25\% \pm 0.24\%$	0.59% 1.09%	$0.19\% \pm 0.16\%$	$-6.98\% \pm 7.52\%$	-29.2% ± 1.52%	$-0.86\% \pm 0.05\%$	$0.19\% \pm 0.16\%$
PA66	$7.42\% \pm 0.74\%$	-26.7% ± 51.8%	$5.49\% \pm 0.55\%$	$1.55\% \pm 1.14\%$	$2.54\% \pm 1.31\%$	$4.00\% \pm 0.21\%$	$4.45\% \pm 1.98\%$
PC	$0.15\% \pm 0.21\%$	$0.39\% \pm 0.25\%$	$-1.58\% \pm 2.65\%$	$-8.24\% \pm 11.0\%$	-59.9% ± 3.97%	-16.1% ± 3.67%	$0.00\% \pm 0.12\%$
PMMA	$1.35\% \pm 0.33\%$	$3.28\%\pm2.73\%$	$1.15\% \pm 0.10\%$	$0.57\% \pm 0.42\%$	$0.54\% \pm 0.10\%$	$0.03\% \pm 0.76\%$	$0.57\% \pm 0.08\%$

b. Size

	Protocol 1a	Protocol 1b	Protocol 2	Protocol 3a	Protocol 3b	Protocol 4	Control
	H_2O_2 (60°C)	H_2O_2 (70°C)	Fenton's reagent	1 M NaOH	10 M NaOH	10% KOH	
PP	$-2.35\% \pm 1.88\%$	$-4.99\% \pm 9.12\%$	$1.66\%\pm4.27\%$	$-3.57\% \pm 2.52\%$	$-1.52\% \pm 4.32\%$	$-3.61\% \pm 4.15\%$	$-0.47\% \pm 3.88\%$
LDPE	$1.64\% \pm 4.13\%$	$-0.61\% \pm 3.64\%$	$0.50\%\pm3.20\%$	$-3.38\% \pm 1.20\%$	$-1.02\% \pm 3.53\%$	$-2.26\% \pm 3.59\%$	$-0.24\% \pm 4.61\%$
HDPE	$\textbf{-0.79\%} \pm 2.38\%$	$-1.13\% \pm 2.27\%$	$1.26\% \pm 2.23\%$	$-2.57\% \pm 0.23\%$	$-0.95\% \pm 3.06\%$	$-3.53\% \pm 2.82\%$	$1.58\% \pm 1.46\%$
PS	$-2.41\% \pm 4.22\%$	$3.34\% \pm 5.77\%$	$-0.27\% \pm 3.23\%$	$-2.40\% \pm 0.26\%$	$-0.95\% \pm 2.60\%$	$-4.42\% \pm 4.37\%$	$\textbf{-0.80\%} \pm 4.76\%$
PET	$-0.68\% \pm 5.32\%$	$0.18\% \pm 4.13\%$	$1.79\%\pm2.38\%$	$-0.88\% \pm 1.52\%$	$-10.4\% \pm 6.37\%$	$-3.13\% \pm 5.53\%$	$-0.31\% \pm 3.09\%$
PA66	$-0.78\% \pm 3.35\%$	$-33.4\% \pm 47.2\%$	$2.10\%\pm3.98\%$	$-0.30\% \pm 4.11\%$	$0.20\% \pm 4.26\%$	$2.36\% \pm 4.23\%$	$0.89\% \pm 4.59\%$
PC	$0.10\% \pm 0.06\%$	$-1.33\% \pm 4.64\%$	$2.93\% \pm 6.33\%$	$-3.14\% \pm 1.64\%$	$-27.8\% \pm 7.13\%$	$-4.70\% \pm 5.36\%$	$0.17\% \pm 3.95\%$
PMMA	$-0.82\% \pm 3.60\%$	$-1.08\% \pm 3.90\%$	$1.54\% \pm 2.46\%$	$-2.21\% \pm 0.03\%$	$-3.28\% \pm 4.43\%$	$-3.87\% \pm 2.80\%$	$-3.60\% \pm 4.74\%$

Table 2. Total mass loss following treatment (Phase 2 testing) and the corresponding proportion of organic material removed for each of the tested protocols for sludge (a) and soil (b). Results are presented as the mean of the three replicates \pm SD.

a. Sludge

	Mass loss	Organic matter removal
Protocol 1a H ₂ O ₂ (60°C)	$41.3\% \pm 2.16\%$	$80.2\% \pm 4.20\%$
Protocol 1b H ₂ O ₂ (70°C)	$44.6\% \pm 6.76\%$	$86.6\% \pm 13.1\%$
Protocol 2 Fenton's	$43.8\% \pm 6.61\%$	$86.9\% \pm 9.87\%$
Protocol 3a 1 M NaOH	$31.4\% \pm 2.88\%$	$60.9\% \pm 5.60\%$
Protocol 3b 10 M NaOH	$34.6\pm3.01\%$	$67.2\% \pm 5.84\%$
Protocol 4 10% KOH	$29.2\pm8.56\%$	$56.8\% \pm 16.6\%$

b. Soil

	Mass loss	Organic matter removal		
Protocol 1a	6 54% + 1 01%	96 3% + 14 9%		
H ₂ O ₂ (60°C)	0.0170 ± 1.0170	90.970±11.970		
Protocol 1b	$7.36\% \pm 0.74\%$	108% + 10.9%		
H_2O_2 (70°C)	7.50/0 ± 0.74/0	100/0 ± 10.9/0		
Protocol 2	$6.81\% \pm 1.56\%$	106% + 13.8%		
Fenton's	$0.01/0 \pm 1.00/0$	10070±13.870		
Protocol 3a	1 50% + 1 30%	67 6% + 20 59		
1 M NaOH	$4.39/0 \pm 1.39/0$	07.070 ± 20.370		
Protocol 3b	$438\% \pm 200\%$	61 104 + 12 70		
10 M NaOH	$4.30/0 \pm 2.90/0$	04.470 ± 42.770		
Protocol 4	22404 ± 15204	24 50/ + 22 50/		
10% KOH	2.3470 ± 1.3370	$54.5\% \pm 22.5\%$		



Figure 2. Extraction efficiencies for three microplastic types following treatment (Protocol 2: Fenton's reagent) and density separation. The extraction method was tested as 1) organic matter removal (OMR) followed by density separation, and 2) Density separation followed by organic matter removal. Results are reported as the mean of the three replicates \pm SD.

ASSOCIATED CONTENT

Supporting Information. Details of the experimental design; details of the polymeric material used in the study including the fibre production method; information regarding the test sludge and soil samples including the control assessment for microplastic content; FT-IR spectra of the analysed particles; results of the extraction efficiency studies.

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Notes

The authors declare no competing financial interest.

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